

# Managing Thermal Gradients on a Supercritical Carbon Dioxide Radial Inflow Turbine

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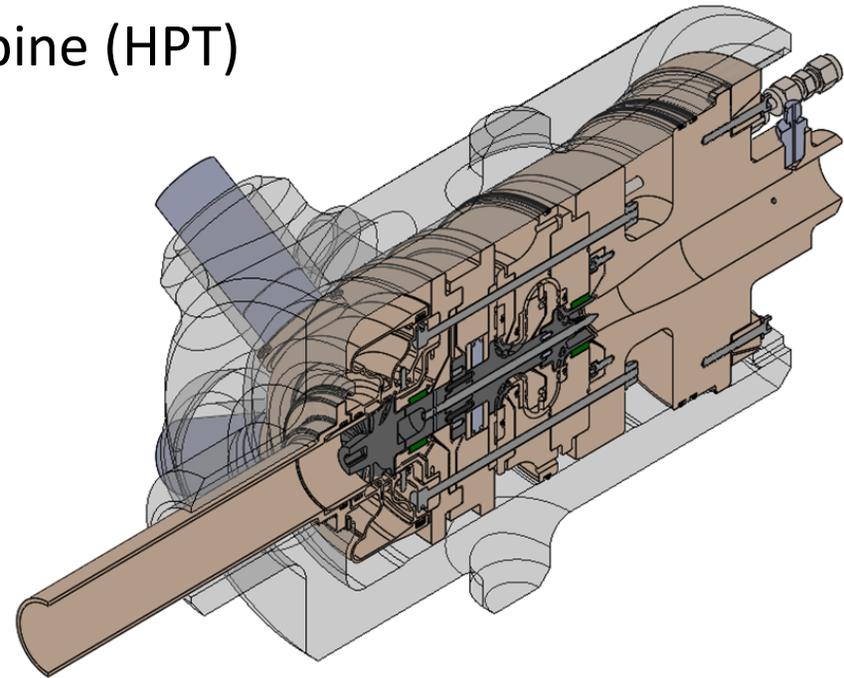


**PEREGRINE**  
TURBINE TECHNOLOGIES

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- Historically, a consistent engineering challenge
- Machine durability
- Traditional gas turbines:
  - Turbine inlet temperatures as high as 1600°C (2912°F)
  - Beyond melting point of metal turbine materials
  - Secondary flows are routinely used to cool components
    - Sophisticated air cooling passages employed on blades
- SCO<sub>2</sub> Turbomachines:
  - Turbine inlet temperatures are currently limited to 750°C (1382°F)
    - Primary heat exchanger
  - Challenges originate from the unique thermo-physical heat transfer properties of SCO<sub>2</sub>

- Two stage centrifugal compressor
- Single stage radial high pressure turbine (HPT)
- $W_0 = 12.1 \text{ lbm/s}$
- $T_2 = 194^\circ\text{F}$
- $P_2 = 6220 \text{ psi}$
- $T_3 = 1382^\circ\text{F}$
- $P_3 = 6000 \text{ psi}$



- Steady state and transient thermal analysis performed
- Results revealed engineering challenge contrary to traditional air cooled machines
- Strong thermal gradients through back face of HPT caused by overcooling
- Overcooling caused by unique thermo-physical properties of SCO<sub>2</sub>
- Resulting structural analysis revealed stresses beyond fatigue design criteria
- Unique secondary flow cooling method was developed to correct the problem

- Typical temperature and pressures of air and SCO<sub>2</sub> machines are as different as the physical properties themselves
  - Traditional gas turbine:
    - T<sub>1</sub>, P<sub>1</sub> ≈ Ambient
    - P<sub>2</sub> ≈ 400 psi
    - T<sub>2</sub> ≈ 1000°F
    - T<sub>3</sub> ≈ 2900°F (Max)
  - Peregrine 1 MW turbo pump:
    - P<sub>1</sub> = 1100 psi
    - T<sub>1</sub> = 90°F
    - P<sub>2</sub> = 6220 psi
    - T<sub>2</sub> = 194°F
    - T<sub>3</sub> = 1382°F

- Root of the problem is high heat transfer coefficients produced by the unique thermo-physical properties of SCO<sub>2</sub>
  - Examine how differences in thermo-physical properties effect fundamental convective heat transfer equations and dimensionless quantities
  - In context of typical operating temperatures and pressures of each machine type.
- Properties:
  - dynamic viscosity  $\mu$
  - thermal conductivity  $k$
  - density  $\rho$
  - specific heat  $c_p$
- Dimensionless Quantities:
  - Reynolds Number  $Re$
  - Prandtl Number  $Pr$
  - Nusselt Number  $Nu$

# Relevant Equations

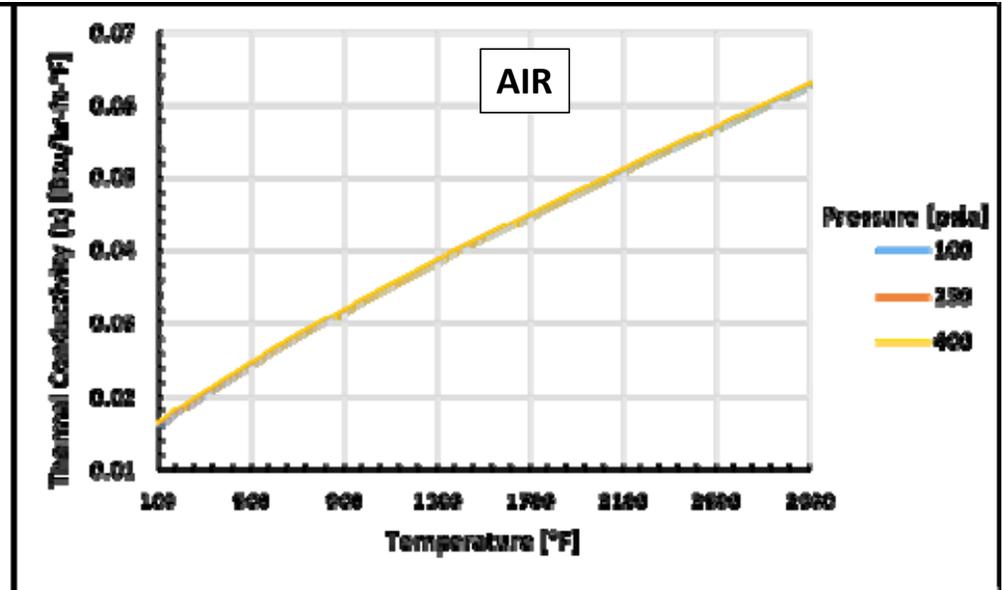
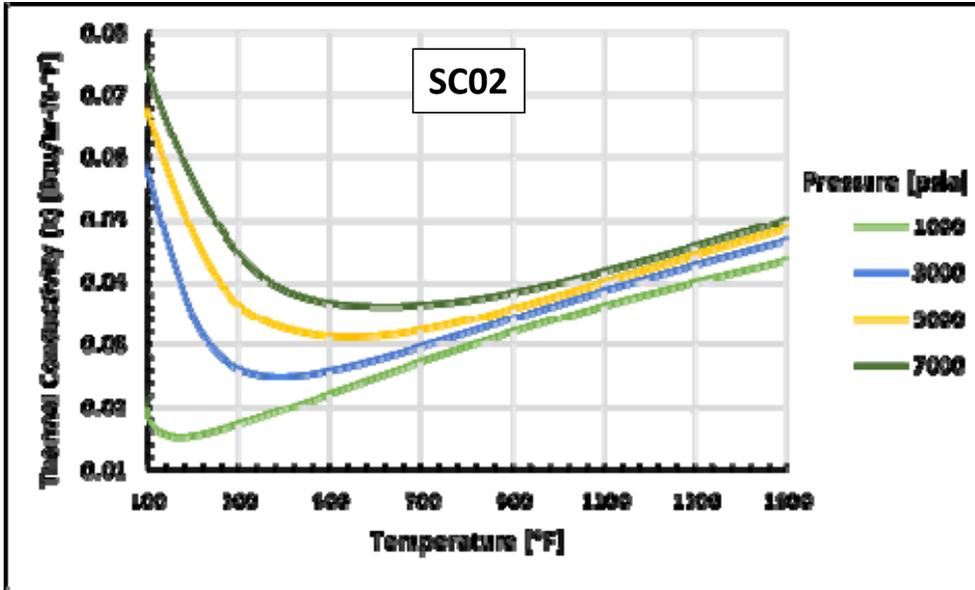
$$\text{Reynolds Number: } Re = \frac{\text{Inertial forces}}{\text{Viscous forces}} = \frac{\rho v L_c}{\mu}$$

$$\text{Prandtl Number: } Pr = \frac{\text{Molecular diffusivity of momentum}}{\text{Molecular diffusivity of heat}} = \frac{\mu c_p}{k}$$

$$\text{*Nusselt Number: } Nu = \frac{h L_c}{k} = 0.023 Re^{0.8} Pr^{1/3} \text{ for } \left\{ \begin{array}{l} 0.5 \leq Pr \leq 160 \\ Re \geq 10^4 \end{array} \right\}$$

*\*Chilton Colburn equation used for comparison purposes only.  
Actual correlations used in thermal model beyond scope of paper*

# Thermal Conductivity



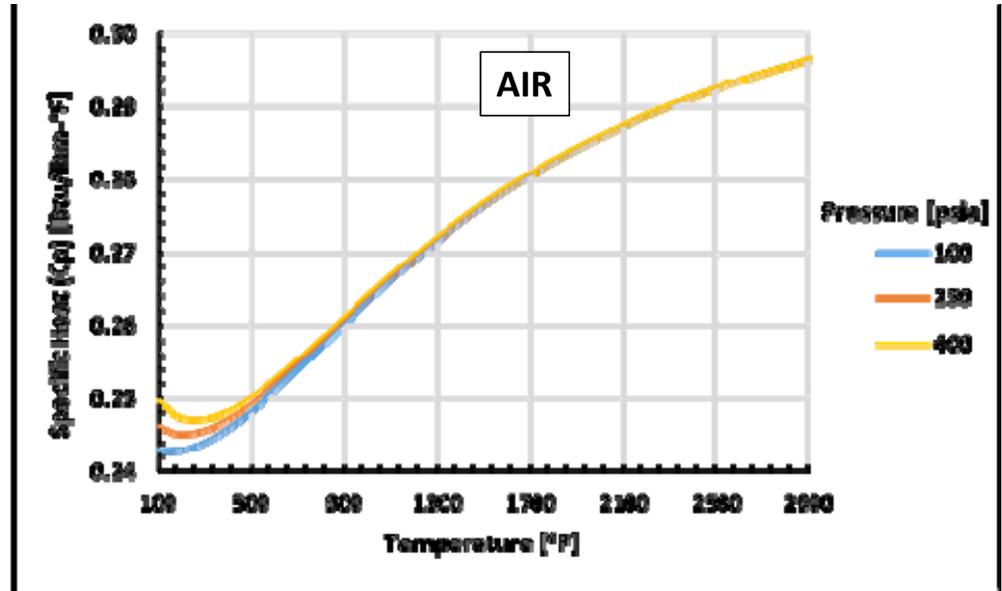
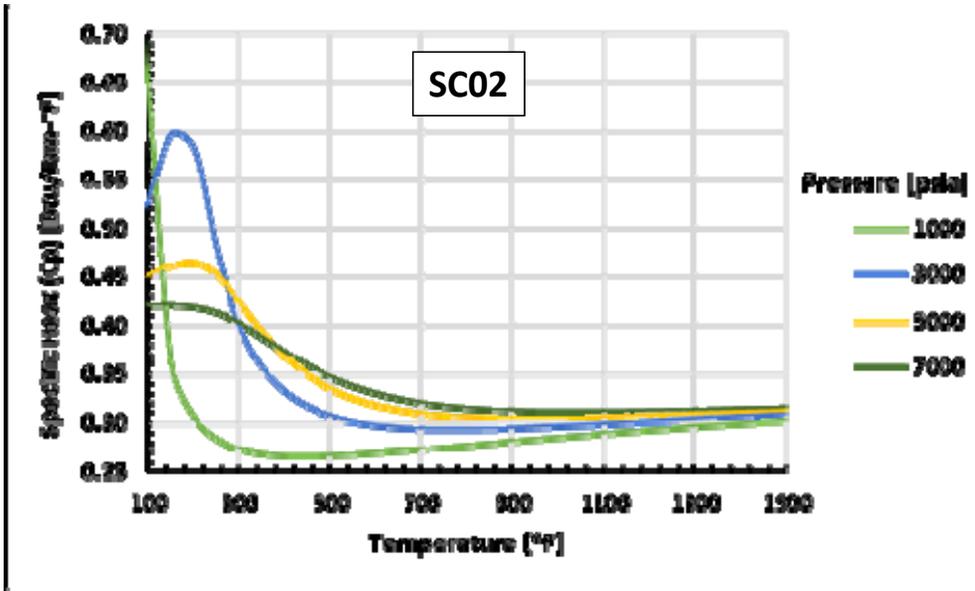
## Compressor Discharge Conditions

|                    | Pressure [psia] | Temperature [°F] | Thermal Conductivity (k) [Btu/hr-ft-°F] |
|--------------------|-----------------|------------------|---|
| PTT 1MW Turbo Pump | 6220            | 194              | 0.054                                   |
| Air Gas Turbine    | 400             | 1000             | 0.034                                   |



**Thermal conductivity of SC02 1.5x greater than air**

# Specific Heat

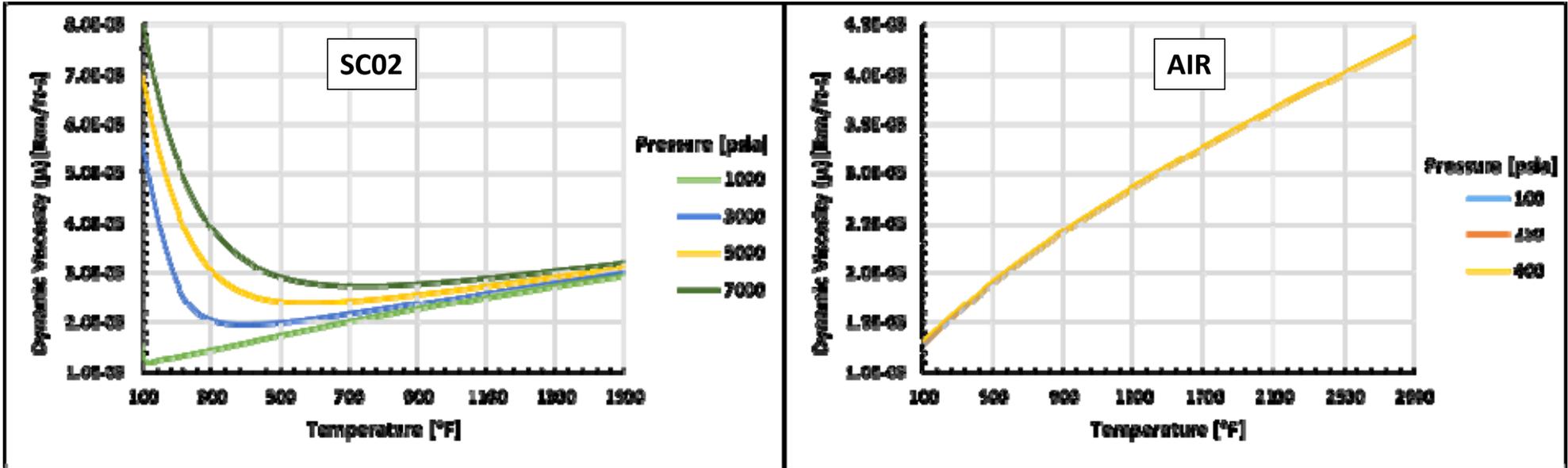


## Compressor Discharge Conditions

|                    | Pressure<br>[psia] | Temperature<br>[°F] | Specific Heat (Cp)<br>[Btu/lbm-°F] |
|--------------------|--------------------|---------------------|------------------------------------|
| PTT 1MW Turbo Pump | 6220               | 194                 | 0.433                              |
| Air Gas Turbine    | 400                | 1000                | 0.264                              |

Specific heat of SC02 2x greater than air

Higher heat transfer capacity of fluid



### Compressor Discharge Conditions

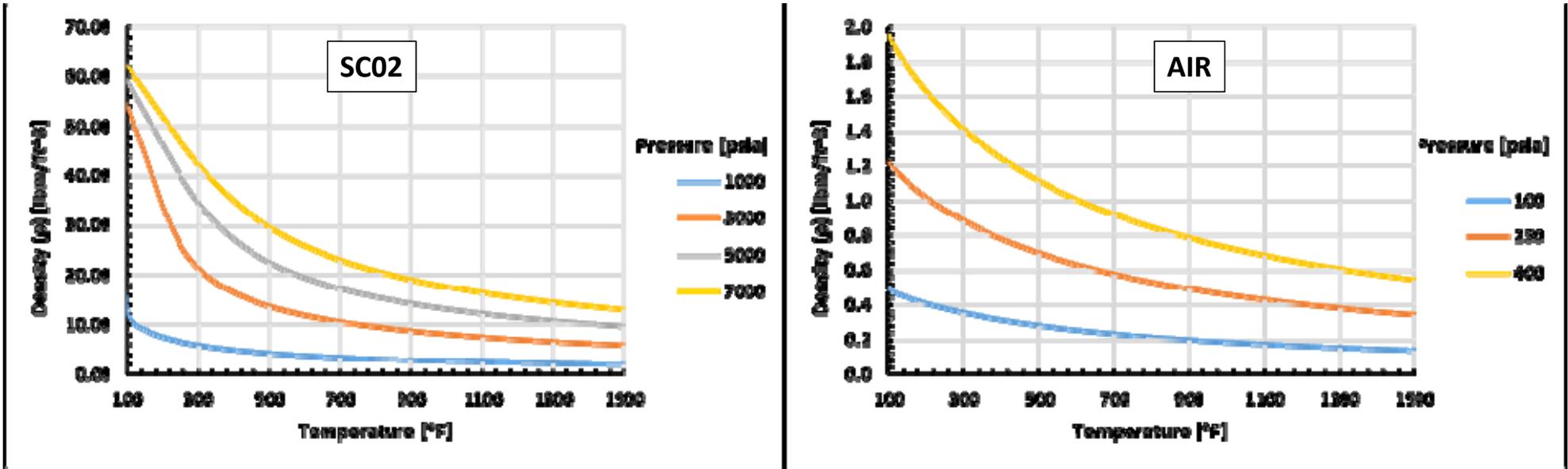
|                    | Pressure [psia] | Temperature [°F] | Dynamic Viscosity ( $\mu$ ) [lbm/ft-s] |
|--------------------|-----------------|------------------|--|
| PTT 1MW Turbo Pump | 6220            | 194              | 4.97E-05                               |
| Air Gas Turbine    | 400             | 1000             | 2.55E-05                               |



Dynamic viscosity of SC02 2x greater than air



Decrease in Reynolds Number  
Increase in Prandtl Number



### Compressor Discharge Conditions

|                    | Pressure [psia] | Temperature [°F] | Density (ρ) [lbm/ft³] |
|--------------------|-----------------|------------------|-----------------------|
| PTT 1MW Turbo Pump | 6220            | 194              | 50.460                |
| Air Gas Turbine    | 400             | 1000             | 0.733                 |

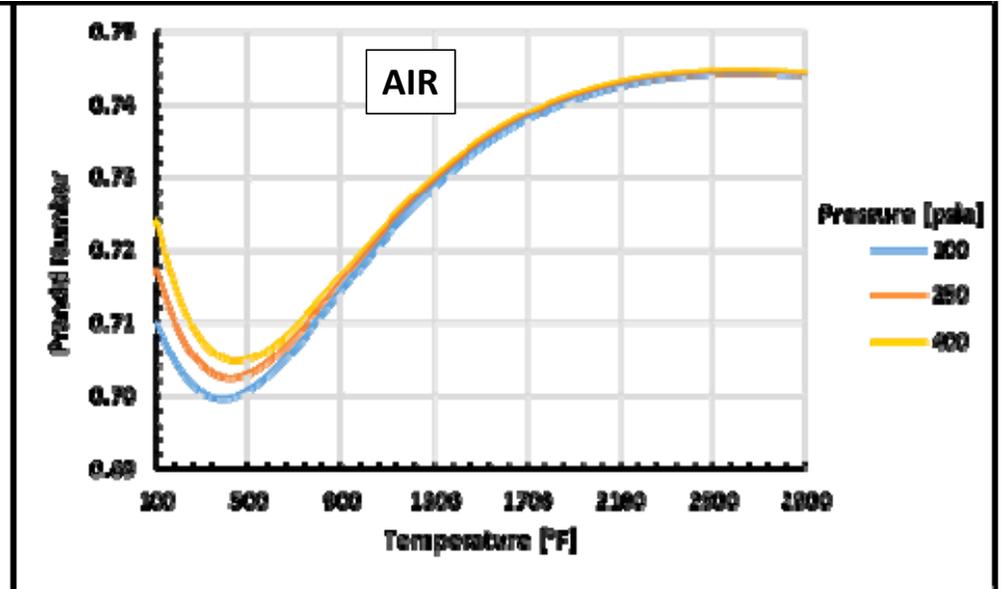
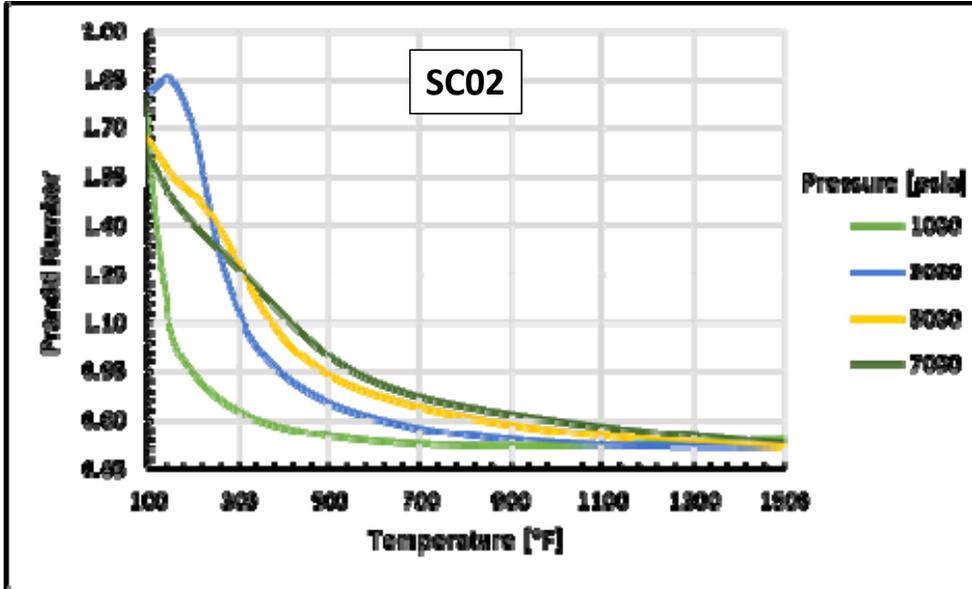


Density of SCO2 70x greater than air



Higher Reynolds Numbers

# Prandtl Number

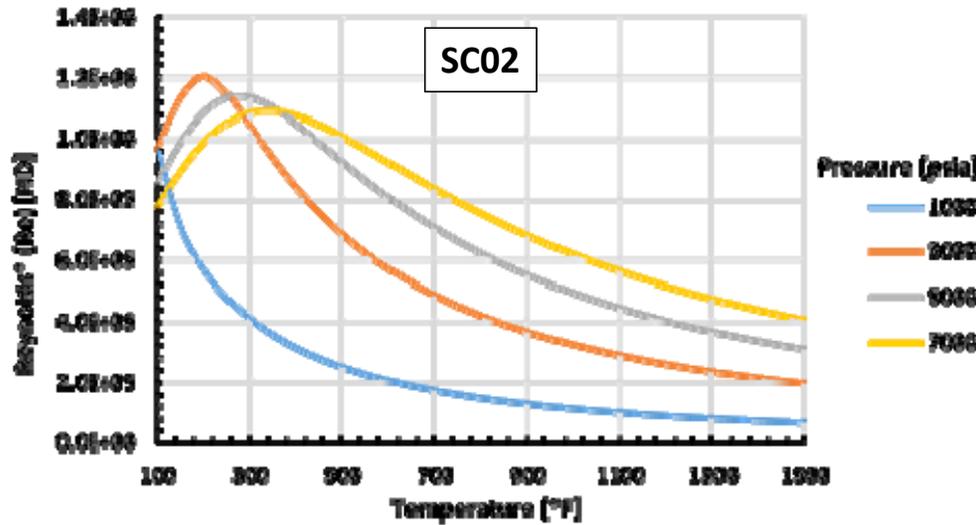


## Compressor Discharge Conditions

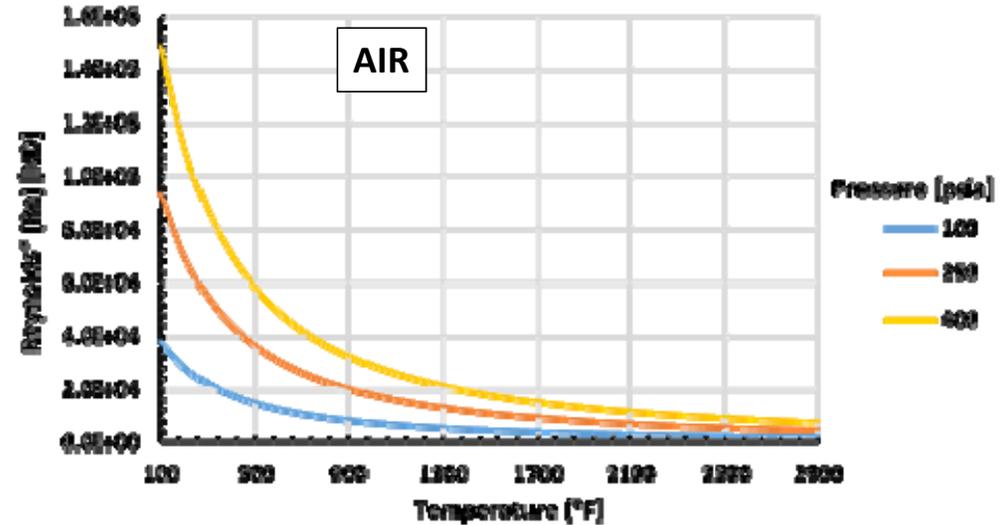
|                    | Pressure [psia] | Temperature [°F] | Prandtl (Pr) [ND] |
|--------------------|-----------------|------------------|-------------------|
| PTT 1MW Turbo Pump | 6220            | 194              | 1.44              |
| Air Gas Turbine    | 400             | 1000             | 0.72              |



**SCO2 will have relatively thinner thermal boundary layer**  
**Pr > 1: Convection Dominated**  
**Pr < 1: Conduction Dominated**



\*Assuming  $r^*$  and  $L_r$  are constant and equal to 1 respectively



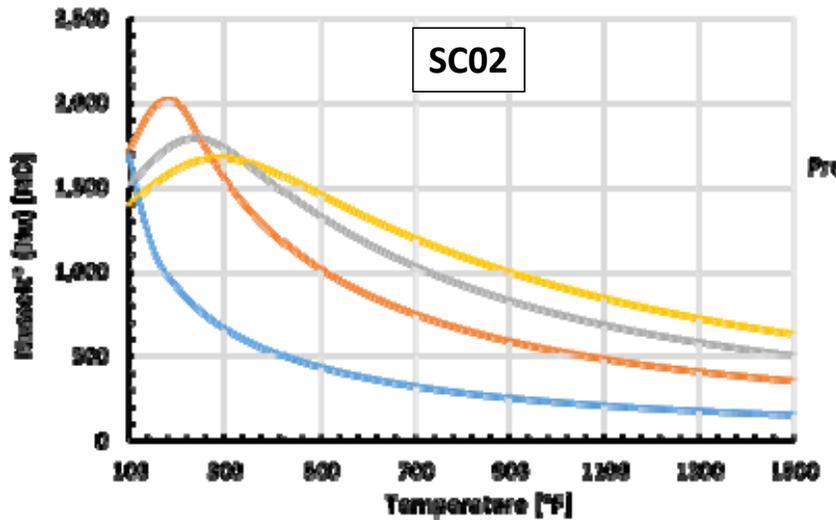
\*Assuming  $r^*$  and  $L_r$  are constant and equal to 1 respectively

### Compressor Discharge Conditions

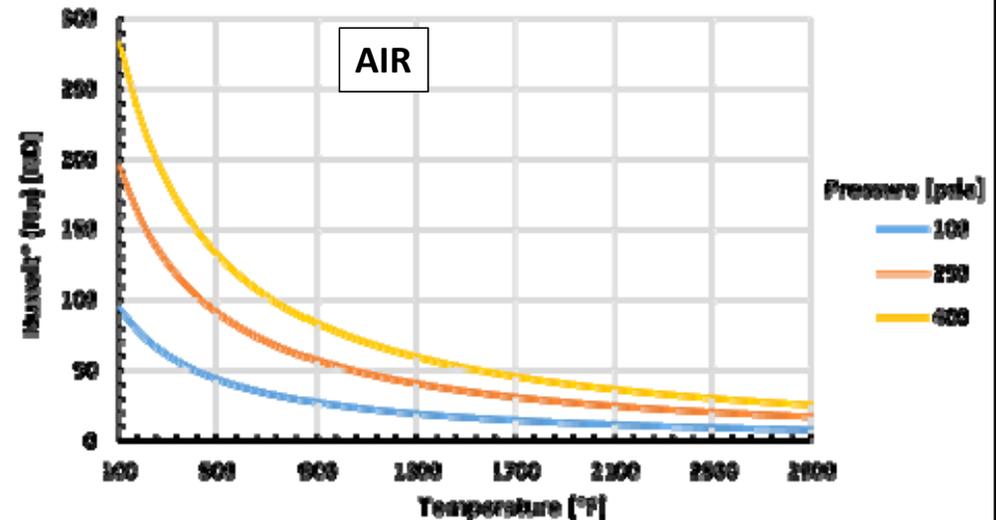
|                    | Pressure [psia] | Temperature [°F] | Reynolds (Re) [ND] |
|--------------------|-----------------|------------------|--------------------|
| PTT 1MW Turbo Pump | 6220            | 194              | 1.02E+06           |
| Air Gas Turbine    | 400             | 1000             | 2.88E+04           |



**Reynolds Number of SC02 35x greater than air**



\*Assuming  $\nu$  and  $f_{sc}$  are constant and equal to 1 respectively



\*Assuming  $\nu$  and  $f_{sc}$  are constant and equal to 1 respectively

## Compressor Discharge Conditions

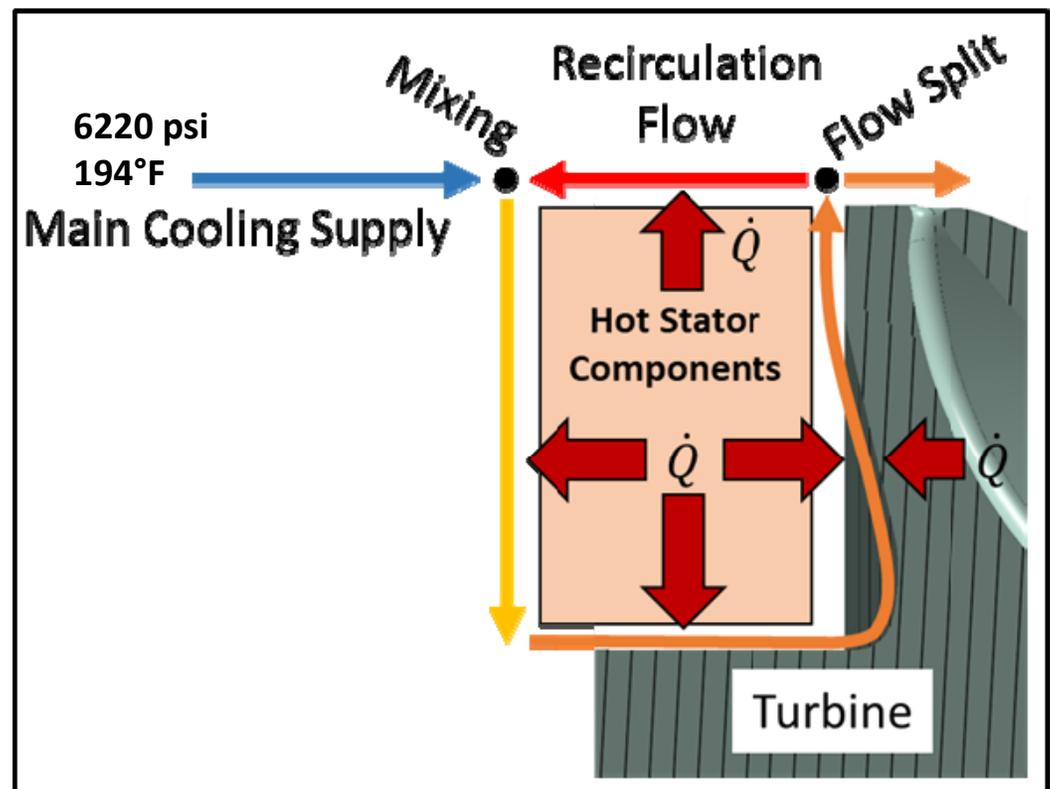
|                    | Pressure [psia] | Temperature [°F] | Nusselt (Nu) [ND] |
|--------------------|-----------------|------------------|-------------------|
| PTT 1MW Turbo Pump | 6220            | 194              | 1659              |
| Air Gas Turbine    | 400             | 1000             | 76                |



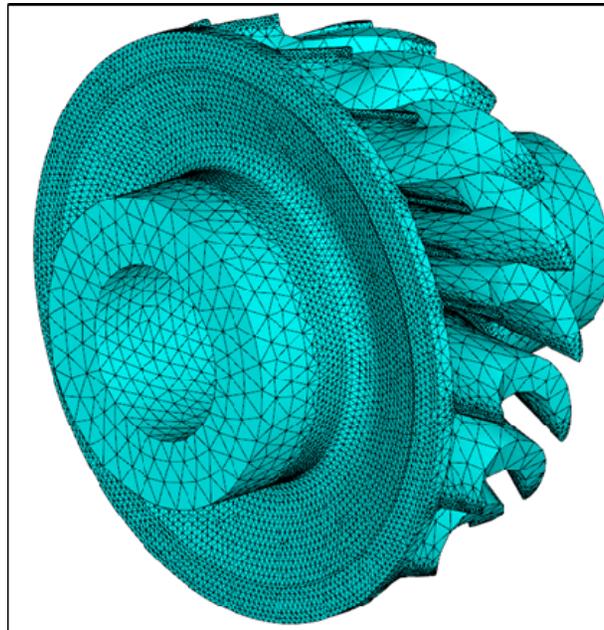
**Nusselt Number of SCO2 22x greater than air**

- Significantly higher Nusselt numbers in SCO<sub>2</sub> indicate highly convection dominated heat transfer coefficients.
- Surface temperatures on HPT will be driven close to mean fluid temperatures
- Thermal tug of war between heating of HPT primary flow surfaces and turbine back face
- Steep thermal gradient on turbine back face

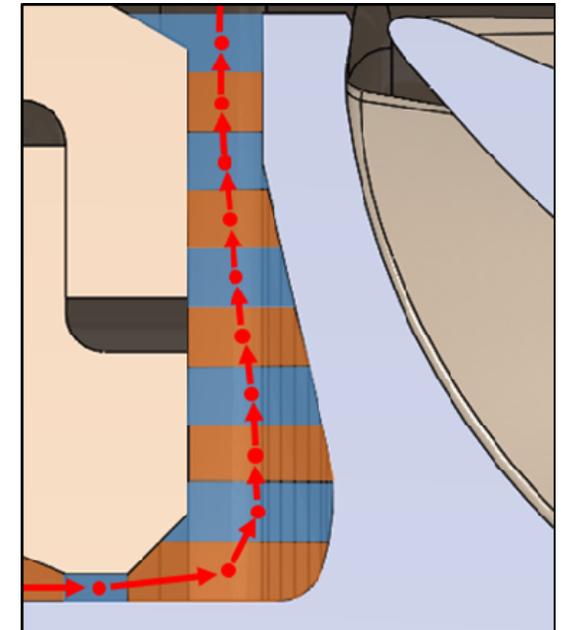
- Reduce cooling mass flow rate?
  - Very low already
  - Bearing cooling concerns
- Reduce Nusselt number/ HTC?
  - Inherent to fluid properties
- ✓ Raise temperature of cooling flow
  - Preheat cooling flow using high temperature stator components



- ANSYS APDL
- Ten node tetrahedral solid elements
- FLUID 116 Elements
- Model Inputs:
  - Aerodynamic analysis results
  - Secondary flow analysis results
- Common model of transient and steady state



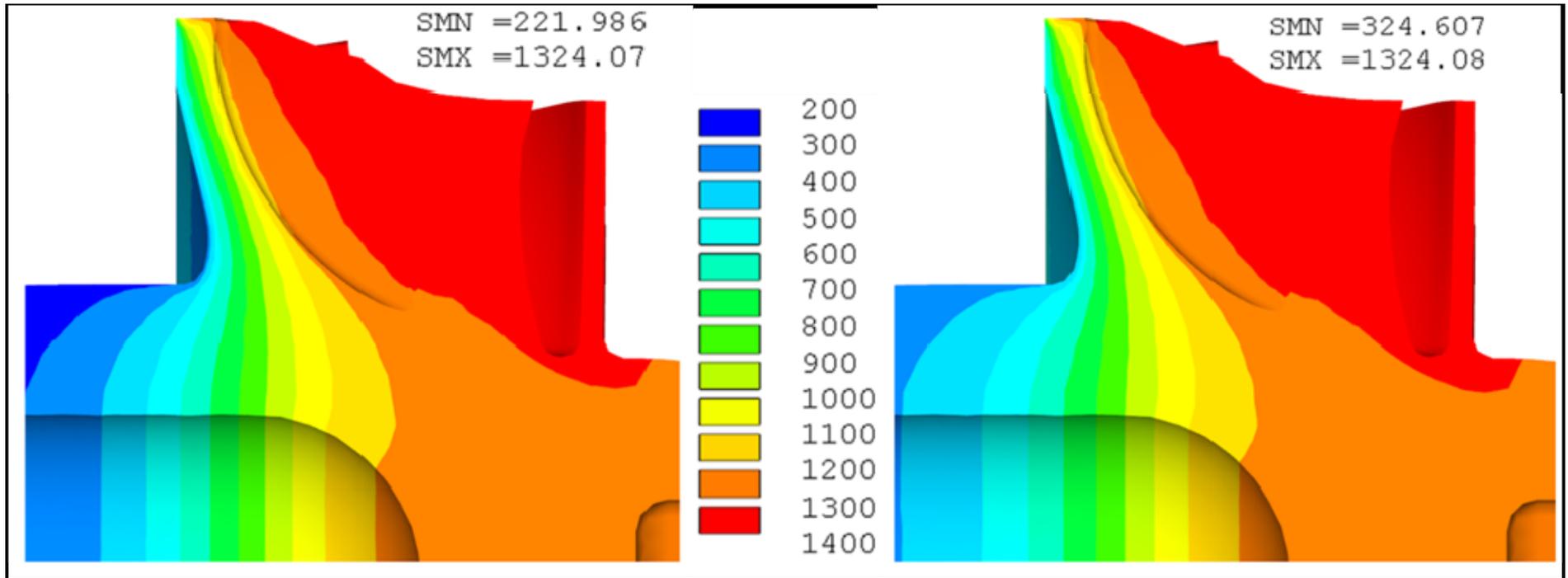
HPT solid body thermal mesh



HPT back face fluid network

- ANSYS
- Ten node tetrahedral solid elements
- Model Inputs:
  - Thermal model results
  - Angular velocity
  - Surface pressures
  - Assembly loads

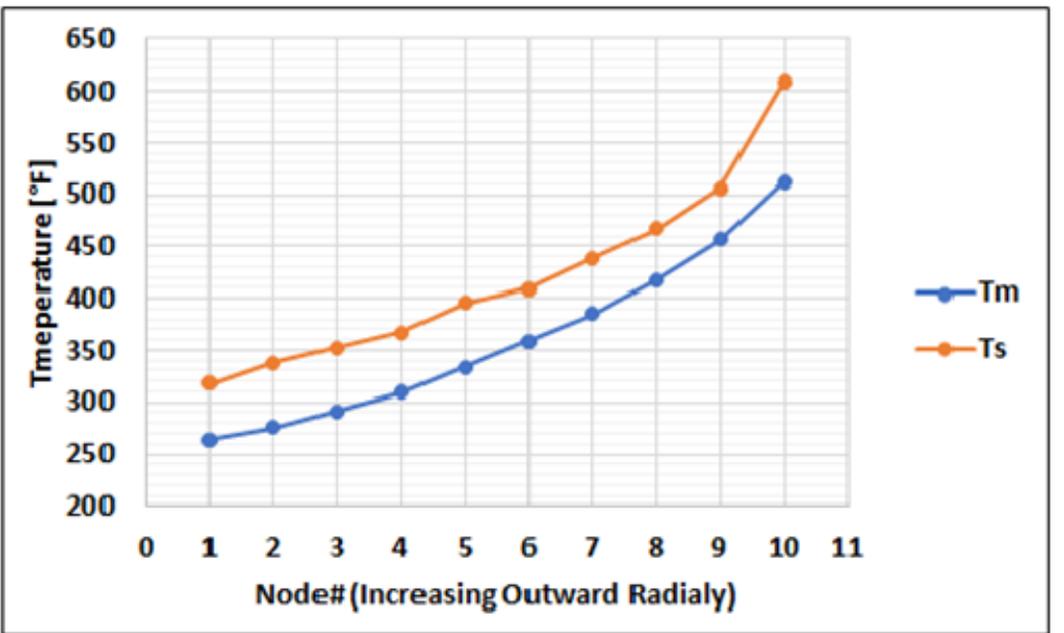
# Thermal Model Results



SS max HPT isothermal Plot (°F). No recirculation flow left. With recirculation flow right. (SMN and SMX are maximum and minimum temperatures)

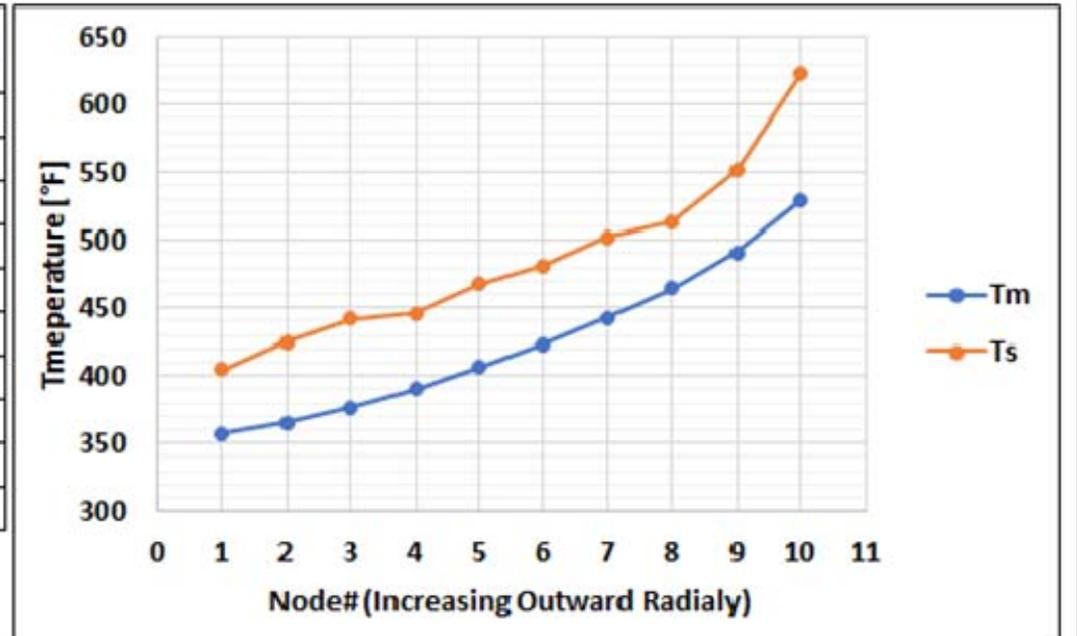
# Thermal Model Results

| Location |        | Temperature [°F] |        | $\Delta T$<br>(Ts-Tm) | % Difference |
|----------|--------|------------------|--------|-----------------------|--------------|
| #        | r [in] | Tm               | Ts     |                       |              |
| 1        | 0.447  | 264.13           | 317.26 | 53.13                 | 18%          |
| 2        | 0.473  | 275.80           | 338.00 | 62.21                 | 20%          |
| 3        | 0.531  | 291.64           | 352.95 | 61.31                 | 19%          |
| 4        | 0.565  | 309.71           | 367.36 | 57.65                 | 17%          |
| 5        | 0.603  | 333.88           | 395.54 | 61.66                 | 17%          |
| 6        | 0.641  | 358.25           | 409.50 | 51.25                 | 13%          |
| 7        | 0.680  | 385.43           | 438.13 | 52.70                 | 13%          |
| 8        | 0.717  | 417.47           | 467.26 | 49.79                 | 11%          |
| 9        | 0.759  | 456.08           | 505.93 | 49.85                 | 10%          |
| 10       | 0.797  | 511.65           | 609.01 | 97.36                 | 17%          |

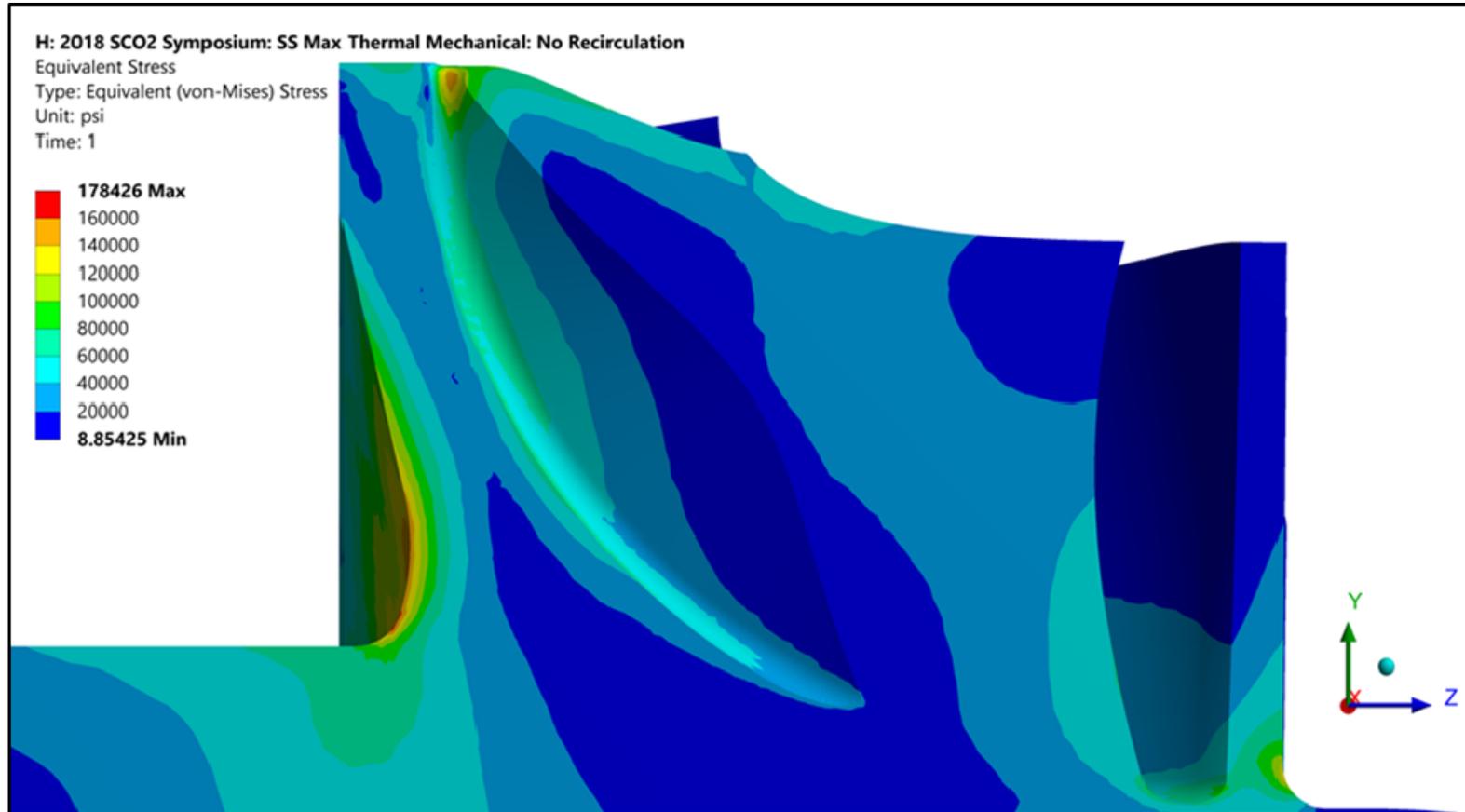


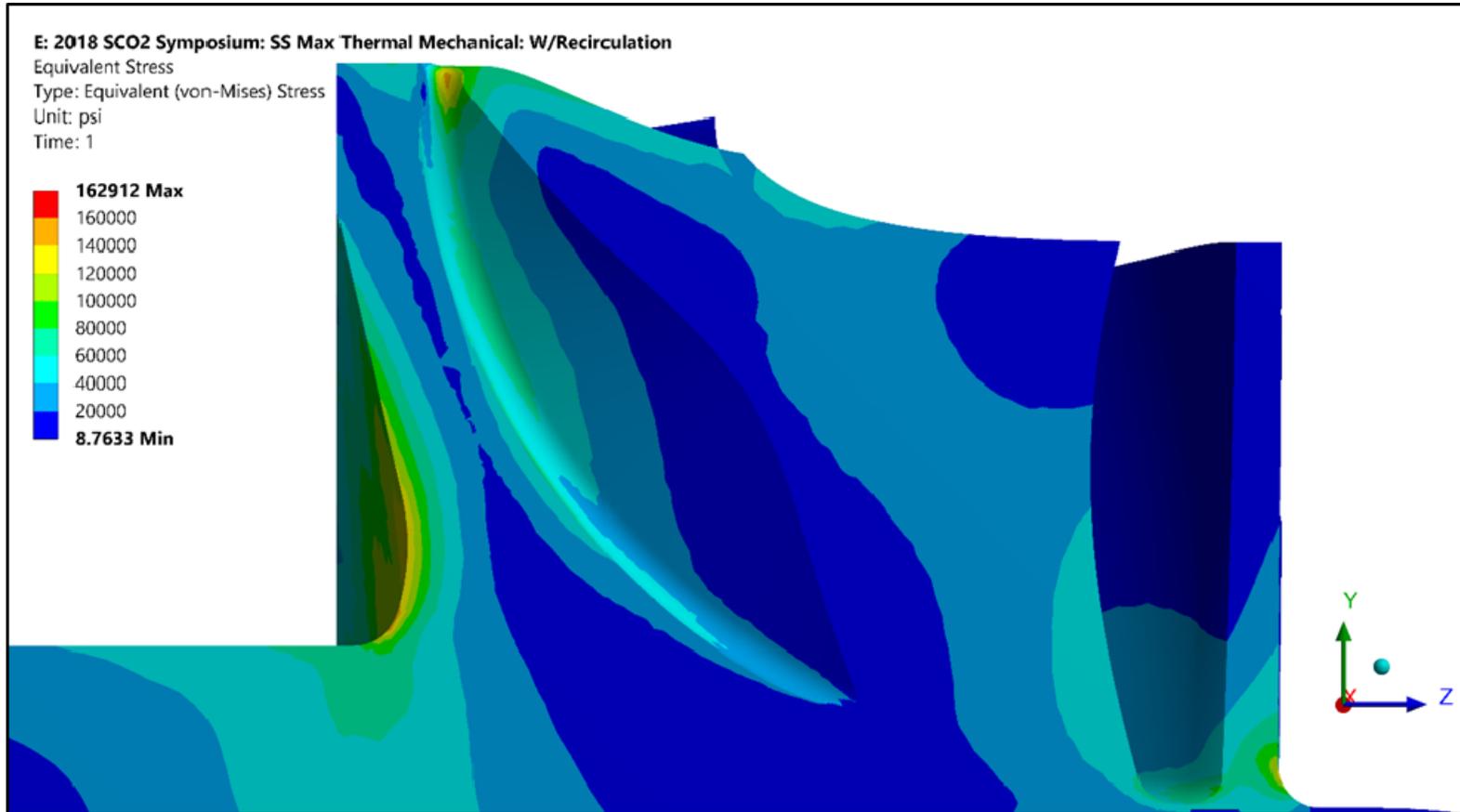
SS max HPT back face temperatures fluid vs. surface (no recirculation flow)

| Location # | r [in] | Temperature [°F] |        | $\Delta T$<br>(Ts-Tm) | % Difference |
|------------|--------|------------------|--------|-----------------------|--------------|
|            |        | Tm               | Ts     |                       |              |
| 1          | 0.447  | 356.97           | 404.52 | 47.55                 | 12%          |
| 2          | 0.473  | 365.76           | 425.02 | 59.26                 | 15%          |
| 3          | 0.531  | 376.96           | 441.55 | 64.58                 | 16%          |
| 4          | 0.565  | 390.00           | 445.68 | 55.68                 | 13%          |
| 5          | 0.603  | 406.20           | 467.81 | 61.62                 | 14%          |
| 6          | 0.641  | 423.64           | 481.56 | 57.92                 | 13%          |
| 7          | 0.680  | 442.81           | 502.03 | 59.22                 | 13%          |
| 8          | 0.717  | 464.87           | 513.47 | 48.60                 | 10%          |
| 9          | 0.759  | 491.45           | 551.93 | 60.47                 | 12%          |
| 10         | 0.797  | 529.53           | 623.58 | 94.05                 | 16%          |



SS max HPT back face temperatures fluid vs. surface (with recirculation flow)





- Problem and solution were contrary to traditional air cooled radial turbine wheels
- The root of the problem was high thermal gradients caused by high convective heat transfer on the primary flow and back face surfaces of the HPT.
- By examining and discussing how  $s\text{CO}_2$  and air perform very differently as heat transfer media in turbomachinery the problem was directly linked to the unique thermo-physical properties of  $s\text{CO}_2$ .
- Examination revealed Nusselt numbers in typical  $s\text{CO}_2$  turbomachinery can be over 20x greater than in typical air breathing machines.
- A unique and successful secondary flow solution comprised of a preheating recirculation loop was described.
- Stresses were reduced to acceptable fatigue design criteria.